

**AMENDMENTS TO THE CLAIMS**

1. (Original) A process for preparing riboflavin of the B/C modification in granule form, wherein riboflavin of the A modification
  - a) is dissolved in aqueous mineral acid,
  - b) is precipitated directly afterwards, without initially treating the resulting ribo-flavin solution in mineral acid with activated carbon, steps a) and b) being carried out at a temperature in the range from 5 to 15°C, and
  - c) the riboflavin is dried by fluidized bed spray granulation,  
and wherein the riboflavin does not come into contact with the aqueous mineral acid solvent for longer than on average 4 h.
2. (Original) The process according to claim 1, wherein the dissolution temperature is selected within the range from 5 to 12°C.
3. (Currently amended) The process according to claim 1 either of claims 1 and 2, wherein the riboflavin does not come into contact with the aqueous mineral acid solvent for longer than on average 3 h.
4. (Currently amended) The process according to claim 1 any of claims 1 to 3, wherein the precipitation is carried out within a temperature range from 6 to 12°C.
5. (Currently amended) The process according to claim 1 any of claims 1 to 4, wherein the precipitation is carried out continuously.

6. (Currently amended) The process according to claim 1 ~~any of claims 1 to 5~~, wherein the precipitation is carried out in a two-stage stirred tank battery.
7. (Currently amended) The process according to claim 1 ~~any of claims 1 to 6~~, wherein the precipitation is carried out in the first stirred tank of the two-stage stirred tank battery with an average residence time of the riboflavin solution in the first stirred tank of from 1 to 10 min.
8. (Currently amended) The process according to claim 1 ~~any of claims 1 to 7~~, wherein drying is carried out using a continuous or semicontinuous fluidized bed spray granulation in top-spray configuration.
9. (Currently amended) The process according to claim 1 ~~any of claims 1 to 8~~, wherein the temperature of the dry gas blown into the dryer in the fluidized bed spray granulation is in the range from 100 to 200°C.
10. (Currently amended) The process according to claim 1 ~~any of claims 1 to 9~~, wherein the temperature of the dry gas blown into the dryer in the fluidized bed spray granulation is in the range from 150 to 170°C.
11. (Currently amended) The process according to claim 1 ~~any of claims 1 to 10~~, wherein a portion of the riboflavin obtained after the drying is recycled back into the drying process, and the ratio of the stream recycled into the spray fluidized bed to the stream which is removed from the process as the product of value is from about 1:1 to about 4:1.

12. (New) The process according to claim 2, wherein the riboflavin does not come into contact with the aqueous mineral acid solvent for longer than on average 3 h.
13. (New) The process according to claim 3, wherein the precipitation is carried out within a temperature range from 6 to 12°C.
14. (New) The process according to claim 4, wherein the precipitation is carried out continuously.
15. (New) The process according to claim 5, wherein the precipitation is carried out in a two-stage stirred tank battery.
16. (New) The process according to claim 6, wherein the precipitation is carried out in the first stirred tank of the two-stage stirred tank battery with an average residence time of the riboflavin solution in the first stirred tank of from 1 to 10 min.
17. (New) The process according to claim 7, wherein drying is carried out using a continuous or semicontinuous fluidized bed spray granulation in top-spray configuration.
18. (New) The process according to claim 8, wherein the temperature of the dry gas blown into the dryer in the fluidized bed spray granulation is in the range from 100 to 200°C.

19. (New) The process according to claim 9, wherein the temperature of the dry gas blown into the dryer in the fluidized bed spray granulation is in the range from 150 to 170°C.

20. (New) The process according to claim 10, wherein a portion of the riboflavin obtained after the drying is recycled back into the drying process, and the ratio of the stream recycled into the spray fluidized bed to the stream which is removed from the process as the product of value is from about 1:1 to about 4:1.